

1ª Q | $H_B = 20 - 90499 \cdot Q^2 \rightarrow 3500 \text{ rpm.}$

\downarrow
 m

\downarrow
 $\text{m}^3/\text{h.}$

Sistema → $\left\{ \begin{array}{l} \text{Aço 80} \rightarrow \text{DN} = 2'' \\ H_{est} = 8 \text{ m.} \\ L = 220 \text{ m} \end{array} \right. \left\{ \begin{array}{l} D_{int} = 49,2 \text{ mm.} \\ A = 19 \text{ cm}^2 \end{array} \right.$

\downarrow
 $\frac{V_f^2 - V_i^2}{2g} \approx 0.$

saída de reservatório → $Leg_1 = 0,7 \text{ m}$
 válvula gaveta - Mipel → $Leg_2 = 0,70 \text{ m}$
 válvula de retenção horizontal - Mipel - $Leg_3 = 25 \text{ m}$
 valv. globo reta com guia - Mipel - $Leg_4 = 25 \text{ m.}$
 dois cotovéis fêmeas de 90° - Tupy → $Leg_5 = 2 \times 188 \text{ mm}$
 tê passagem direta da Tupy → $Leg_6 = 9,33 \text{ m}$

$$H_S = H_{est} + \frac{V_f^2 - V_i^2}{2g} + H_{P_{TOTALS}}$$

$$H_S = 8 + f_{2''} \times \frac{(220 + 55,49)}{90492} \times \frac{Q^2}{19,6 \times (19 \times 10^{-4})^2}$$

$$H_S = 8 + f_{2''} \times 79.136.613,77 \times Q^2 \Rightarrow f_{2''} = 0,0195$$

$$\therefore \left\{ \begin{array}{l} H_S = 8 + 1.543.163,969 \times Q^2 \\ \downarrow \\ \text{m} \end{array} \right. \left\{ \begin{array}{l} \rightarrow \text{m}^3/\text{s} \end{array} \right.$$

$$\therefore \left\{ \begin{array}{l} H_S = 8 + 0,1191 \times Q^2 \\ \downarrow \\ \text{m} \end{array} \right. \left\{ \begin{array}{l} \rightarrow \text{m}^3/\text{h} \end{array} \right.$$

ou (0,25)

Rotação reduzida para 3000 rpm pelo inversor de frequência, portanto:

(2)

$$\frac{H_{B3000}}{3000^2} = \frac{H_B}{3500^2} \quad \therefore \boxed{H_B = \left(\frac{3500}{3000}\right)^2 \times H_{B3000}} \quad \text{I}$$

$$\frac{Q_{3000}}{3000} = \frac{Q}{3500} \quad \therefore \boxed{Q = \frac{3500}{3000} \times Q_{3000}} \quad \text{II}$$

Considerando as equações I e II na equação dada para 3500 rpm, resulta:

$$\left(\frac{3500}{3000}\right)^2 \times H_{B3000} = 20 - 0,0499 \times \left(\frac{3500}{3000}\right)^2 \times Q_{3000}^2$$

$$H_{B3000} = \left(\frac{3000}{3500}\right)^2 \times 20 - 0,0499 \times Q_{3000}^2$$

$$\boxed{\begin{array}{l} H_{B3000} \cong 14,7 - 0,0499 \times Q_{3000}^2 \\ \downarrow \\ \text{m} \end{array}} \quad \begin{array}{l} \rightarrow \text{m}^3/\text{h} \\ \Rightarrow (0,25) \end{array}$$

Ponto de trabalho $\Rightarrow H_{B3000} = H_S$

$$14,7 - 0,0499 \times Q_{3000}^2 = 8 + 0,1491 \times Q^2$$

$Q_{3000} = Q = Q_G$, portanto:

$$6,7 = 0,169 \times Q_G^2 \quad \Rightarrow \quad Q_G = \sqrt{\frac{6,7}{0,169}}$$

$$\boxed{Q_G \cong 6,3 \frac{\text{m}^3}{\text{h}}} \quad \begin{array}{l} \uparrow (0,25) \\ \Rightarrow \boxed{H_G = 12,7 \text{ m ou } 12,73 \text{ m}} \rightarrow (0,25) \end{array}$$

$$n_g = \frac{3000 \times \sqrt{6,3/3600}}{\sqrt[4]{12,73}} \cong 18,7 \text{ rpm} \quad \therefore \text{realmente é uma bomba}$$

centrífuga radial $\therefore \psi = 0,0011$ e ③
 aí podemos calcular o fator de Thoma:

$$\sigma = \psi \cdot nq^{4/3} = 0,0011 \cdot (18,7)^{4/3} \approx 0,054598598 \approx \underline{0,0546}$$

$$NPSH_{req} = \sigma \cdot H_B = 0,0546 \cdot 12,7 \Rightarrow NPSH_{req} \approx 0,694 \text{ m}$$

(0,25)

$$\begin{aligned} NPSH_{req} &\approx 0,694 \text{ m} \\ \text{ou} \\ NPSH_{req} &\approx 0,7 \text{ m} \end{aligned}$$

$$nq_{usa} = 52 \cdot 18,7 \approx 972,4 \text{ rpm}$$

$$Q_G = 4,402868 \cdot 6,3 \approx 27,8 \text{ gpm}$$

$$\left. \begin{aligned} 2) \eta_{BG} &\approx 54\% \\ \Rightarrow (0,25) \end{aligned} \right\}$$

$$N_{BG} = \frac{\rho \cdot Q_G \cdot H_{BG}}{\eta_{BG}} = \frac{1000 \cdot 9,8 \cdot (6,3/3600) \cdot 12,7}{0,54}$$

$$N_{BG} \approx 403,4 \text{ W} \Rightarrow (0,25)$$

$$H_{B3500} = 20 - 0,0499 \cdot 6,3^2 \Rightarrow H_{B3500} = 18 \text{ m}$$

$$\eta_{B3500} = -9,7723 \cdot 6,3^2 + 11,598 \cdot 6,3 + 146$$

$$\eta_{B3500} = 54\%$$

o que comprova que

$$\eta_{B3500} \approx \eta_{B3000}$$

$$N_{B3500} = \frac{1000 \cdot 9,8 \cdot (6,3/3600) \cdot 18}{0,54} \approx \underline{571,7 \text{ W}}$$

Portanto o investidor propicia uma redução de aproximadamente 29,4% (0,25)

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2ª Q

Aço 120 $\left\{ \begin{array}{l} D_{int} = 139,7 \text{ mm} \\ A = 153,4 \text{ cm}^2 \end{array} \right. ; L = 90 \text{ m};$
 $D_N = 6''$

$f_{\text{médio}} = 0,026 ;$

$\sum L_{eq} = 50 \text{ m} .$

CURVA DE UMA BOMBA $\Rightarrow H_B = 24,9 - 0,0117 \cdot Q - 0,0149 \cdot Q^2$
 $\downarrow \quad \downarrow$
m 4/s

$N_B \text{ cada bomba} = ?$

1. $H_{est} = 13,5 \text{ m}$ e bombas em paralelo.

$H_s = 13,5 + 0,026 \cdot \frac{(50 + 90)}{0,1397} \times \frac{Q^2}{19,6 \cdot (153,4 \cdot 10^{-4})^2}$

$H_s = 13,5 + 5649,4 \cdot Q^2$
 $\downarrow \quad \quad \quad \downarrow$
m m³/s

ou

$H_s = 13,5 + 5,65 \cdot 10^{-3} Q^2$
 $\downarrow \quad \quad \quad \downarrow$
m 4/s

 $\Rightarrow (0,25)$

BOMBAS ASSOCIADAS EM PARALELO \Rightarrow

$H_{Bap} = 24,9 - 0,0117 \cdot \frac{Q_{ap}}{2} - 0,0149 \cdot \left(\frac{Q_{ap}}{2}\right)^2$

$H_{Bap} = 24,9 - 5,85 \cdot 10^{-3} Q_{ap} - 3,725 \cdot 10^{-3} Q_{ap}^2$

 $\Rightarrow (0,25)$

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PONTO DE TRABALHO:

$$13,5 + 5,65 \times 10^{-3} Q_c^2 = 24,9 - 5,85 \times 10^{-3} Q_{ap} - 3,725 \times 10^{-3} Q_{ap}^2$$

$$9,375 \times 10^{-3} Q_c^2 + 5,85 \times 10^{-3} Q_{ap} - 11,4 = 0$$

$$Q_{c\ op} = \frac{-5,85 \times 10^{-3} + \sqrt{(5,85 \times 10^{-3})^2 + 4 \times 9,375 \times 10^{-3} \times 11,4}}{2 \times 9,375 \times 10^{-3}}$$

$$Q_{c\ op} = 34,6 \text{ L/s}$$

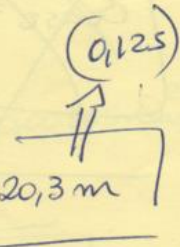
↓
(0,125)

∴ cada bomba contribui com uma vazão de 17,3 L/s ⇒ PARA CADA BOMBA, TEMOS:

$$\eta_{B_c} = 44,2 + 2,8993 \times 17,3 - 0,0779 \times 17,3^2$$

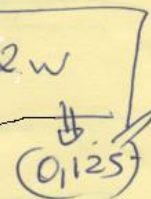
$$\eta_{B_c} = 68\% \rightarrow (0,125)$$

$$N_{B\ cada\ bomba} = \frac{998 \times 9,8 \times (17,3/1000) \times H_B}{0,68}$$



$$H_{B\ ap} = H_{B\ cada\ bomba} = 13,5 + 5,65 \times 10^{-3} \times 34,6^2 \approx 20,3 \text{ m}$$

$$N_{B\ cada\ bomba\ ap} = \frac{998 \times 9,8 \times 17,3 \times 20,3}{0,68 \times 1000} \approx 5051,2 \text{ W}$$



2. $H_{est} = 37,5 \text{ m}$ que é maior que o H_B do shut-off que é $24,9 \text{ m}$, portanto a possibilidade de funcionamento é a associação em série de bombas.

(0,125)

(6)

$$H_{Bas} = 2 \times 24,9 - 2 \times 0,0117 \times Q - 2 \times 0,0149 \times Q^2$$

$$\left[\begin{array}{l} H_{Bas} = 49,8 - 0,0234 \times Q - 0,0298 \times Q^2 \\ \downarrow \qquad \qquad \downarrow \\ m \qquad \qquad \quad \text{40} \end{array} \right] \Rightarrow (0,125)$$

Na equação da CCI, não existe alteração da carga estática, portanto:

$$\left[\begin{array}{l} H_s = 37,5 + 0,00565 \times Q_{as}^2 \\ \downarrow \qquad \qquad \downarrow \\ m \qquad \qquad \quad \text{40} \end{array} \right] \Rightarrow (0,125)$$

No ponto de trabalho:

$$49,8 - 0,0234 \times Q_{as6} - 0,0298 \times Q_{as6}^2 = 37,5 + 0,00565 \times Q_{as6}^2$$

$$0,03545 \times Q_{as6}^2 + 0,0234 Q_{as6} - 12,3 = 0$$

$$Q_{as6} = \frac{-0,0234 + \sqrt{0,0234^2 + 4 \times 0,03545 \times 12,3}}{2 \times 0,03545}$$

$$Q_{as6} = 18,3 \text{ 4/s} \Rightarrow (0,125)$$

$$H_{Bas6} = 37,5 + 0,00565 \times 18,3^2 \Rightarrow H_{Bas6} = 39,4 \text{ m}$$

$$\therefore \left[H_{B\text{cada bomba}} = \frac{39,4}{2} = 19,7 \text{ m} \Rightarrow (0,125) \right]$$

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$$\eta_{Base} = -0,0779 \times 18,3^2 + 2,8993 \times 18,3 + 41,2$$

$$\eta_{Base} = \eta_{Bcada. bomba} \approx 68,2\% \Rightarrow (0,25)$$

$$N_{Bcada. bombas} = \frac{998 \times 9,8 \times 18,3 \times 19,7}{9682 \times 1000} \approx 5170 \text{ W}$$

\Downarrow
(0,25)

$$3^{a} Q \quad H_B = \frac{p_s - p_e}{\gamma} = \frac{788,6 \times 10^3 + 0,258 \times 13600 \times 9,8}{988 \times 9,8}$$

$$H_B \approx 85 \text{ m} \quad (0,5)$$

Pebo gráfico, colocando a origem, temos $p / D_r = 219 \text{ mm} \rightarrow (0,25)$

$$Q_{219} \approx 73,4 \text{ m}^3/\text{h} \rightarrow (0,125)$$

$$H_{B_{219}} \approx 88 \text{ m} \rightarrow (0,125)$$

$$D_r = 219 \times \frac{70}{73,4} \approx 208,9 \text{ mm}$$

$$D_r = 219 \times \sqrt{\frac{70}{73,4}} \approx 213,9 \text{ mm}$$

$$D_r = 219 \times \sqrt{\frac{85}{88}} \approx 215,2 \text{ mm} \leftarrow \text{este o escolhido}$$

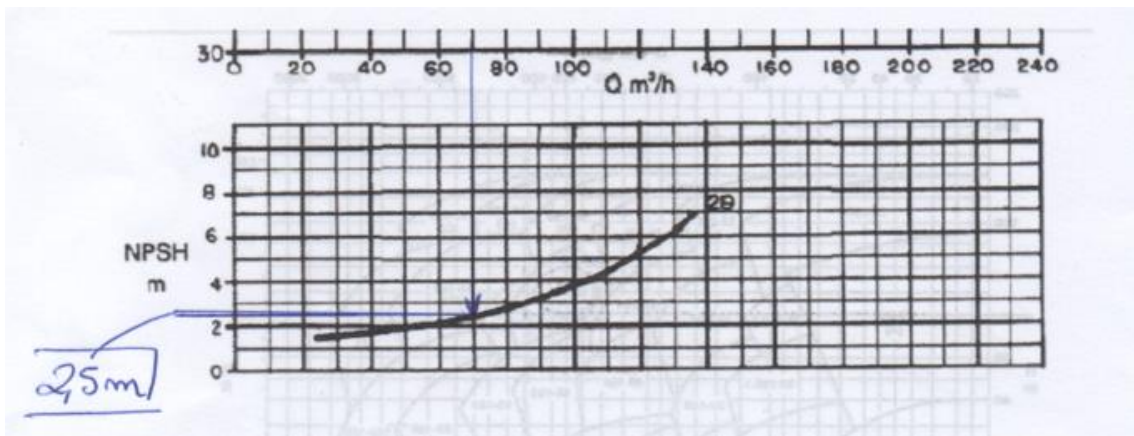
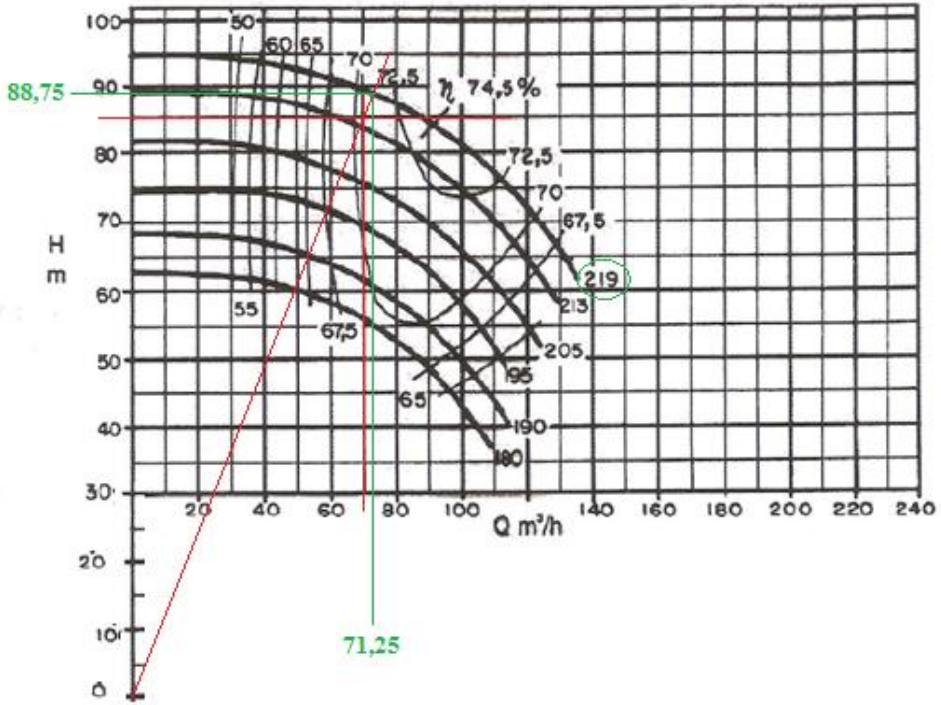
desde que tenha calibração os outros 2 (obris)

(0,5)

Vide gráfico a seguir:

MEGACHEM 50 – 200

3500 rpm



$$NPSH_d = Z_i + \frac{p_{\text{abs}} - p_{\text{vapor}}}{\gamma} - H_{pAB}$$

$$NPSH_d = -2,5 + \frac{95200 - 12262}{988 \times 9,8} - 5,8 \text{ m} = 0,265 \text{ m}$$

$$NPSH_{\text{req}} = 2,5 \text{ m} \rightarrow \text{lido no gráfico.} \Rightarrow (0,25)$$

$$NPSH_d - NPSH_{\text{req}} = 0,265 - 2,5 = -2,235 \text{ m}$$

∞ ESTÁ CAVITANDO ∞ (0,25)

$$\underline{4^a Q} \quad H_L + H_S = H_f + H_{p_{\text{TOTALIS}}} /$$

$$\downarrow$$

$$-3 + H_S = +10 + H_{p_{4''}} + H_{p_{5''}}$$

$$H_S = 13 + H_{p_{5''}} + H_{p_{4''}}$$

$$H_{p_{5''}} = f_{5''} \times \frac{(7 + 5480 + 4,70)}{0,1283} \times \frac{Q^2}{19,6 \times \left[\frac{7 \times 0,1283^2}{4} \right]^2}$$

$$H_{p_{5''}} = f_{5''} \times 158216,7755 \times Q^2 < \begin{cases} f_{5''} = 0,0382 \\ Q = 120 \text{ m}^3/\text{h} \end{cases}$$

$$H_{p_{5''}} = 6,72 \text{ m} \Rightarrow (0,5)$$

$$H_{p4''} = f_{4''} \times \frac{(40 + 3 \times 2,18 + 45,70 + 42,65)}{0,1023} \times \frac{Q^2}{19,6 \times (82,1 \times 10^{-4})^2}$$

$$H_{p4''} = f_{4''} \times 998.071,6859 \times Q^2 \quad \left\{ \begin{array}{l} f_{4''} = 0,0359 \\ 120 \text{ m}^3/\text{h} \end{array} \right.$$

$$H_{p4''} \approx 39,82 \text{ m} \quad (0,5)$$

$$H_s = H_{B \text{ projeto}} = 13 + 6,72 + 39,82$$

$$H_s = 60 \text{ m} \quad \rightarrow \quad H_{B \text{ projeto}} \quad \text{e} \quad Q_{\text{proj}} = 120 \text{ m}^3/\text{h}$$

(0,5)

isto para o fluido viscoso, pois $\gamma = \frac{\mu}{\rho}$

$$\gamma = \frac{0,1}{1530} \approx 6,536 \times 10^{-5} \frac{\text{m}^2}{\text{s}} \approx 65,4 \frac{\text{mm}^2}{\text{s}}, \text{ que}$$

é maior que $20 \text{ mm}^2/\text{s}$ \therefore é fluido viscoso.

Pelo diagrama para fluido viscoso,

$$\text{temos } C_a \approx 0,99 \quad \text{e} \quad C_{H-100} \approx 0,96 \quad (0,125)$$

$$0,99 = \frac{Q_v}{Q_a} \Rightarrow Q_a = \frac{120}{0,99} \approx 121,2 \text{ m}^3/\text{h} \quad (0,125)$$

$$0,96 = \frac{H_{Bv}}{H_{Ba}} \Rightarrow H_{Ba} = \frac{60}{0,96} \approx 62,5 \text{ m} \quad (0,125)$$

Resposta nos diagramas.

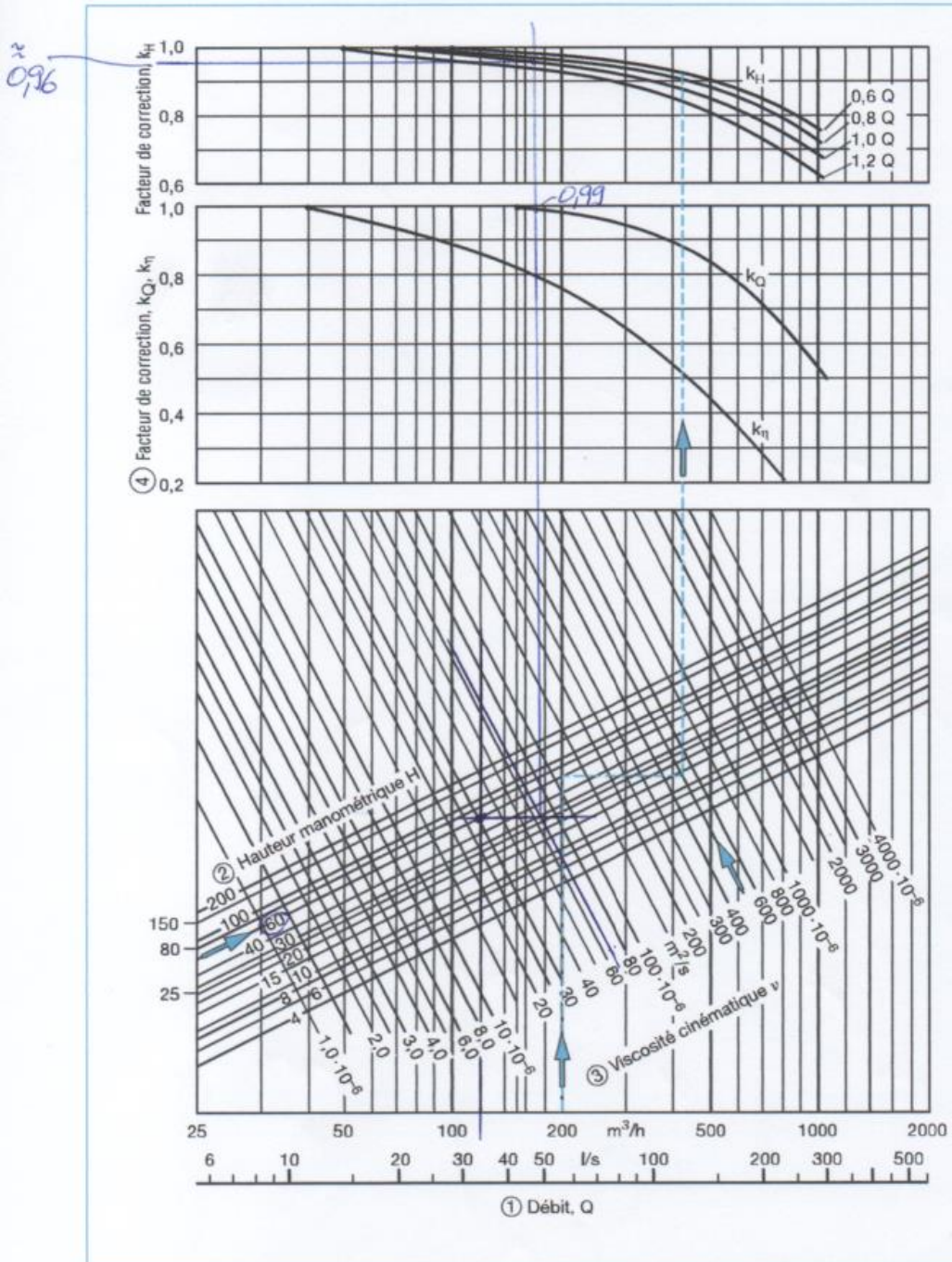
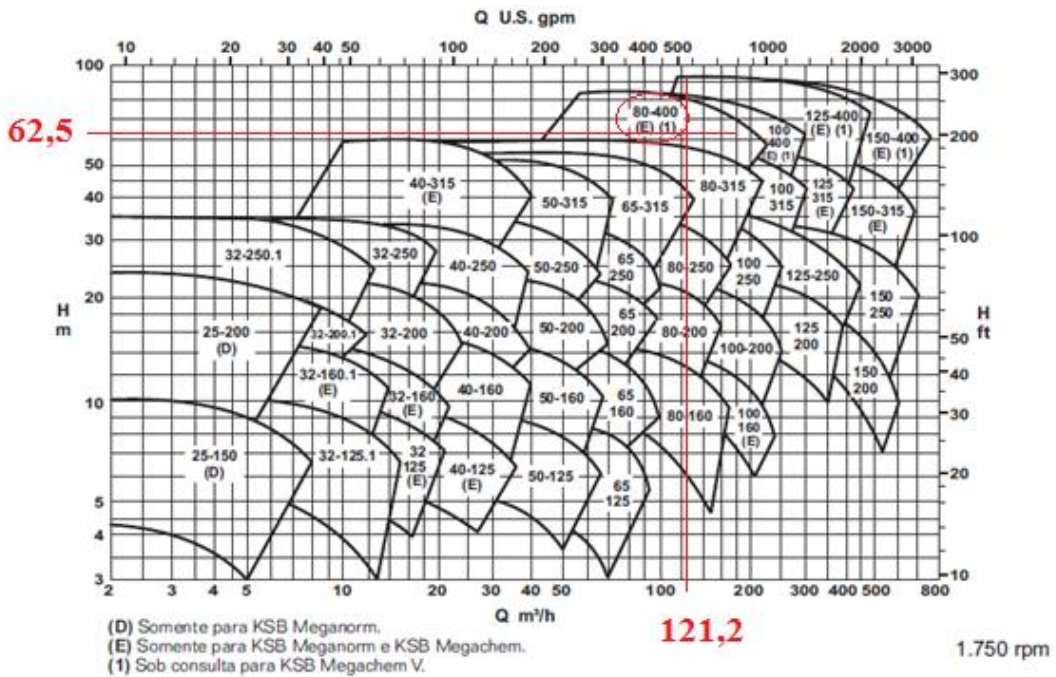
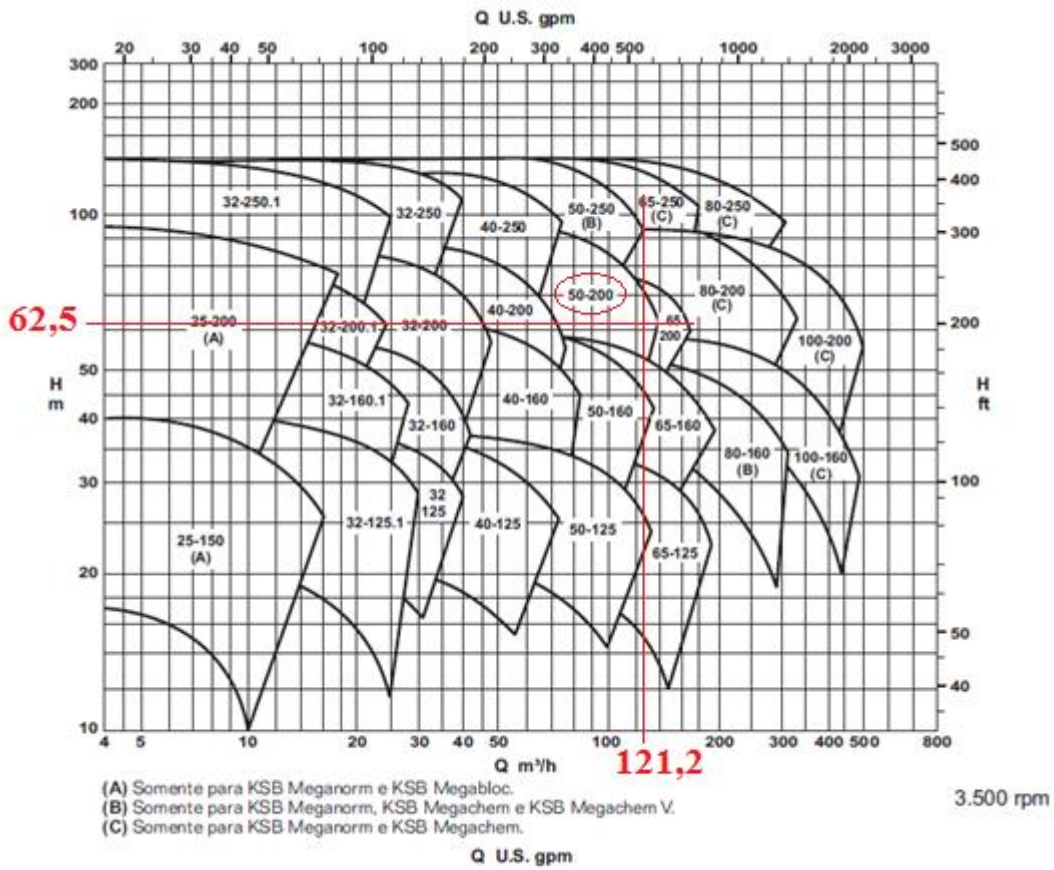


Figure 49 : Détermination des facteurs de correction, k , selon les normes de l'Hydraulic Institute.
Exemple illustré : $Q = 200 \text{ m}^3/\text{h}$, $H = 57,5 \text{ m}$, $\nu = 500 \cdot 10^{-6} \text{ m}^2/\text{s}$



Cada bomba escolhida = 0,25